



Under the Patronage of H.E. the Prime Minister Dr. Mostafa Madbouly



Water Desalination Conference in the Arab Countries

UNDER THE THEME: UNIFYING RESEARCH EFFORTS TO DEVELOP DESALINATION TECHNOLOGIES

23-24 April 2019 • InterContinental City Stars, Cairo, Arab Republic of Egypt



**King Abdulaziz University  
Centre of Excellence in Desalination  
Technology**

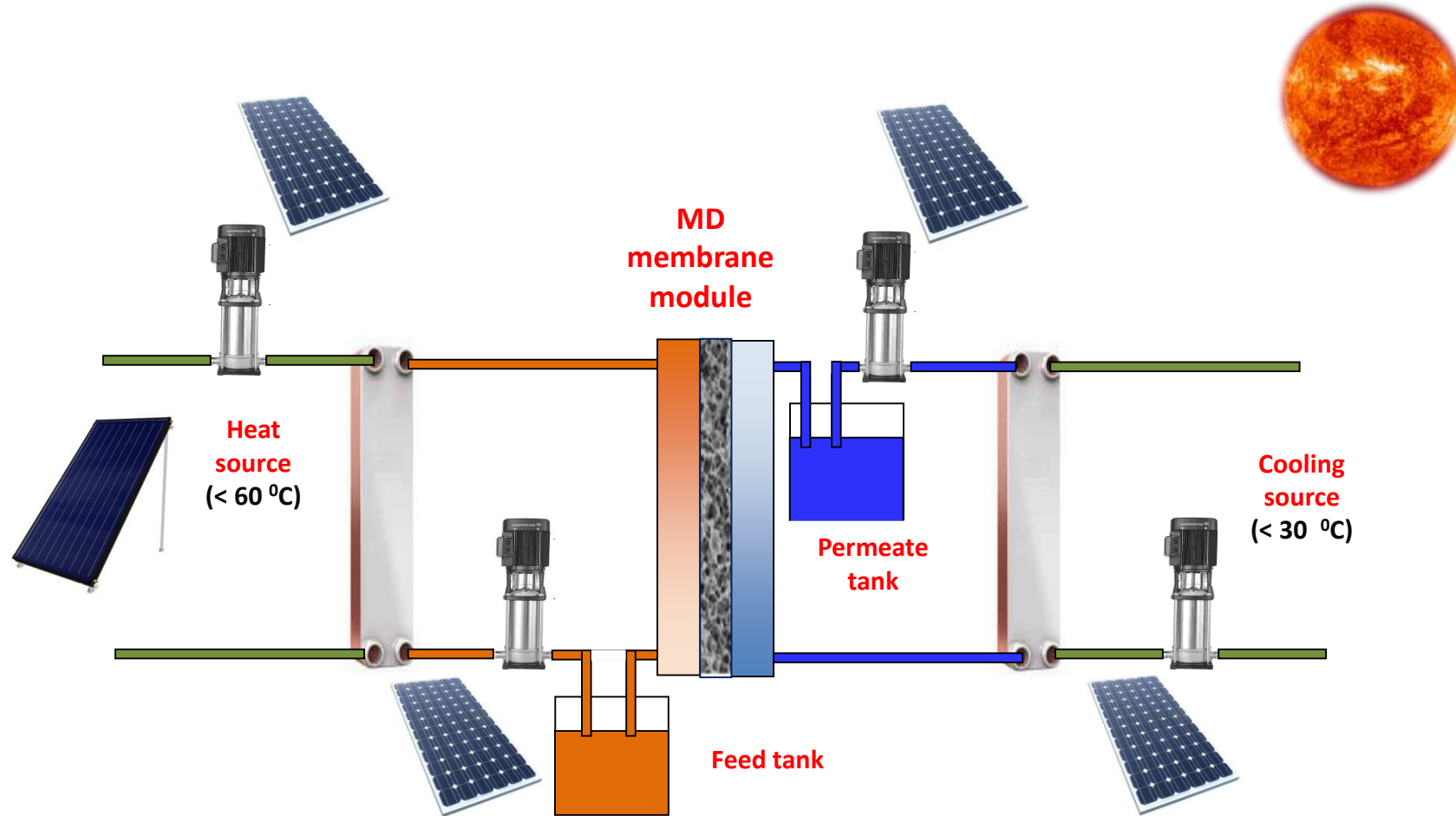


# Effect of Intermittent Operation on Performance of a Solar-Powered Membrane Distillation Pilot Unit

**Mohamad Anas A. Hejazi  
Omar A. Bamaga  
Mohammad H. Al-Beirutty**

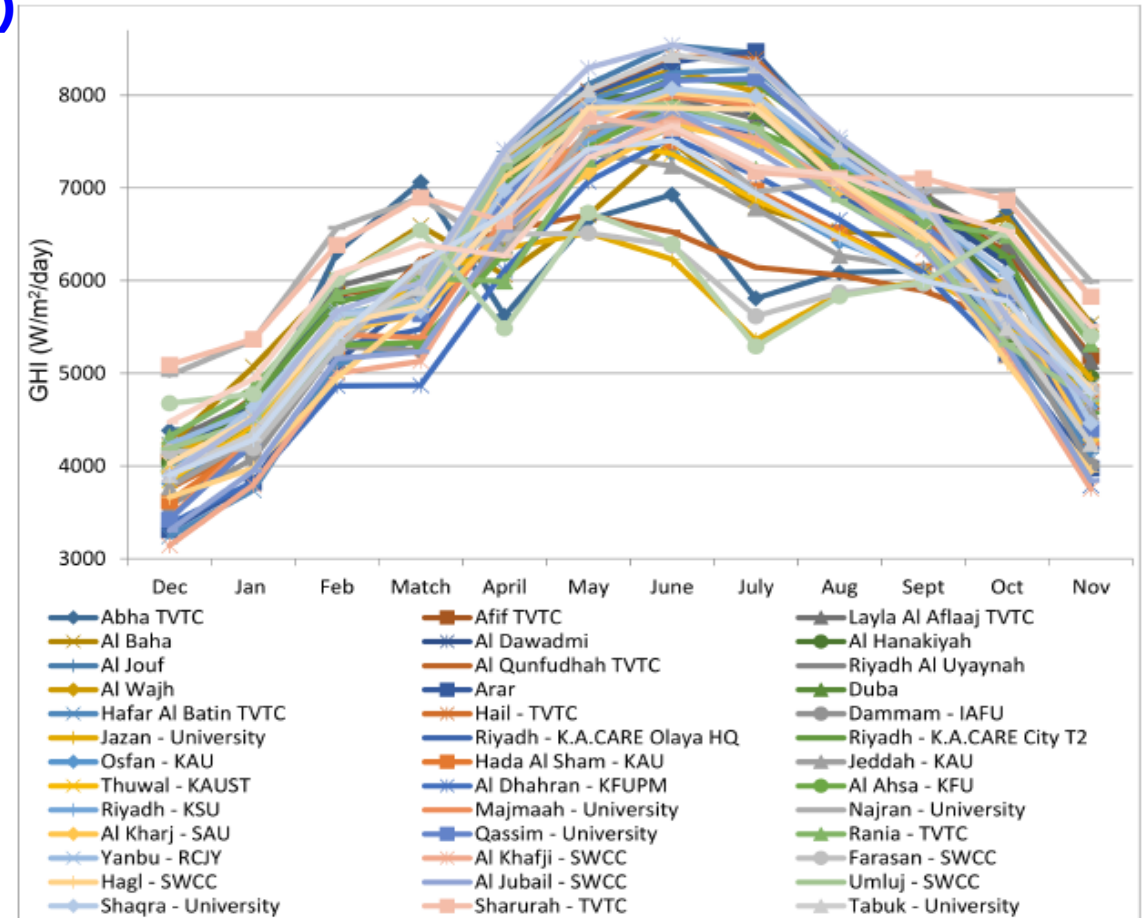
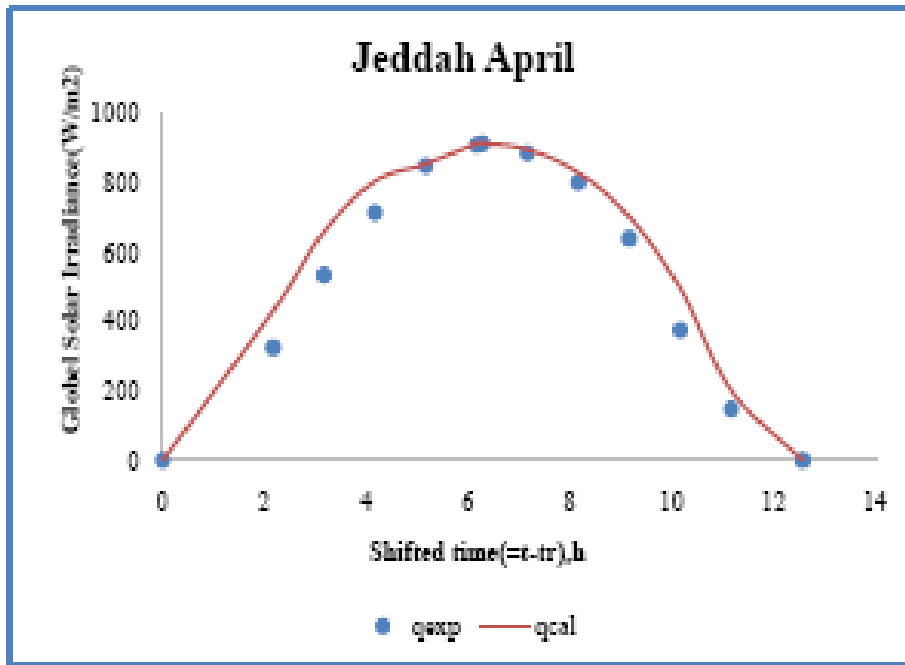


# 1) SPMD system requires both thermal and electrical energy for operation





**Operation of SPMD system is unsteady (depends on variation of solar irradiance throughout the daytime and the year)**



**Experimental and calculated data for Jeddah April**

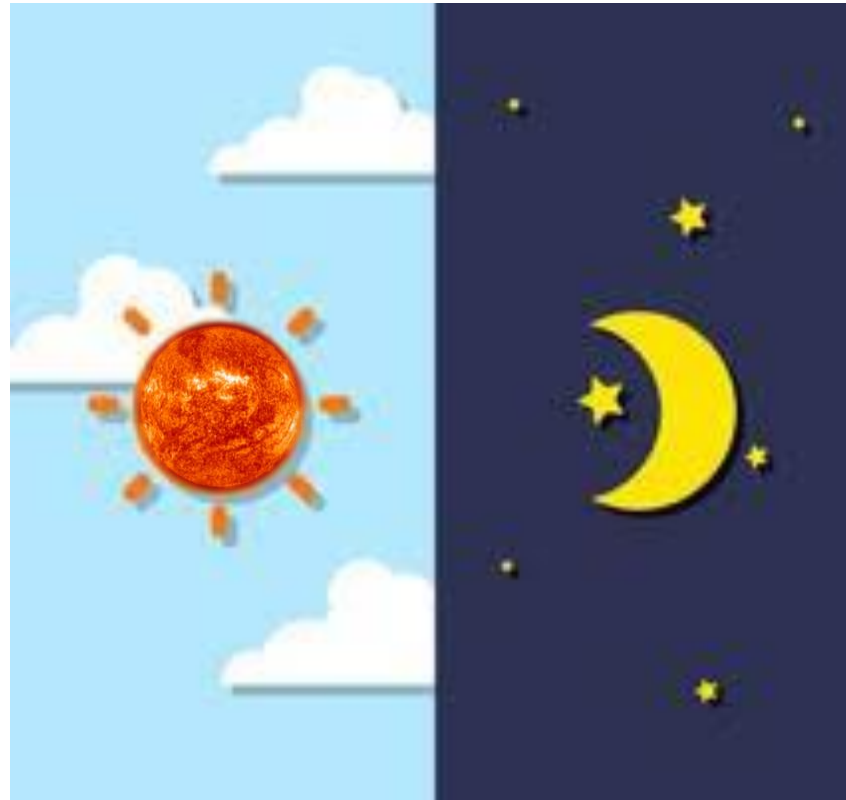
Source: M.K. El-Adawi et. al., International Refereed Journal of Engineering and Science (IRJES) 2015, 4 (6): 85-93

**Average daily total Global Horizontal Irradiance (GHI) of 44 stations over the one-year study period**

Source: Awan et.al. , Sustainability 2018, 10, 1129



**Operation of SPMD system is intermittent (daytime only)**





- *What is the best operation protocol for intermittent operation of SPMD system?*
- *What are the effects of the intermittent operation on the performance of SPMD system?*





# Evaluation of different intermittent operation protocols on bench scale DCMD System



- Three experiments denoted A, B, and C were carried out on a bench-scale DCMD testing unit.
- Each experiment represents a pre-defined operation protocol

**Day-1**  
Feed: Distilled water

**8 days**

**Days-2 to 8**  
Feed: SWRO brine, TDS 55 g/l

**A**

*(Wash and drain protocol):*

The feed channel of the module is washed with a distilled water at the shutdown event, drained, and left to dry overnight

**B**

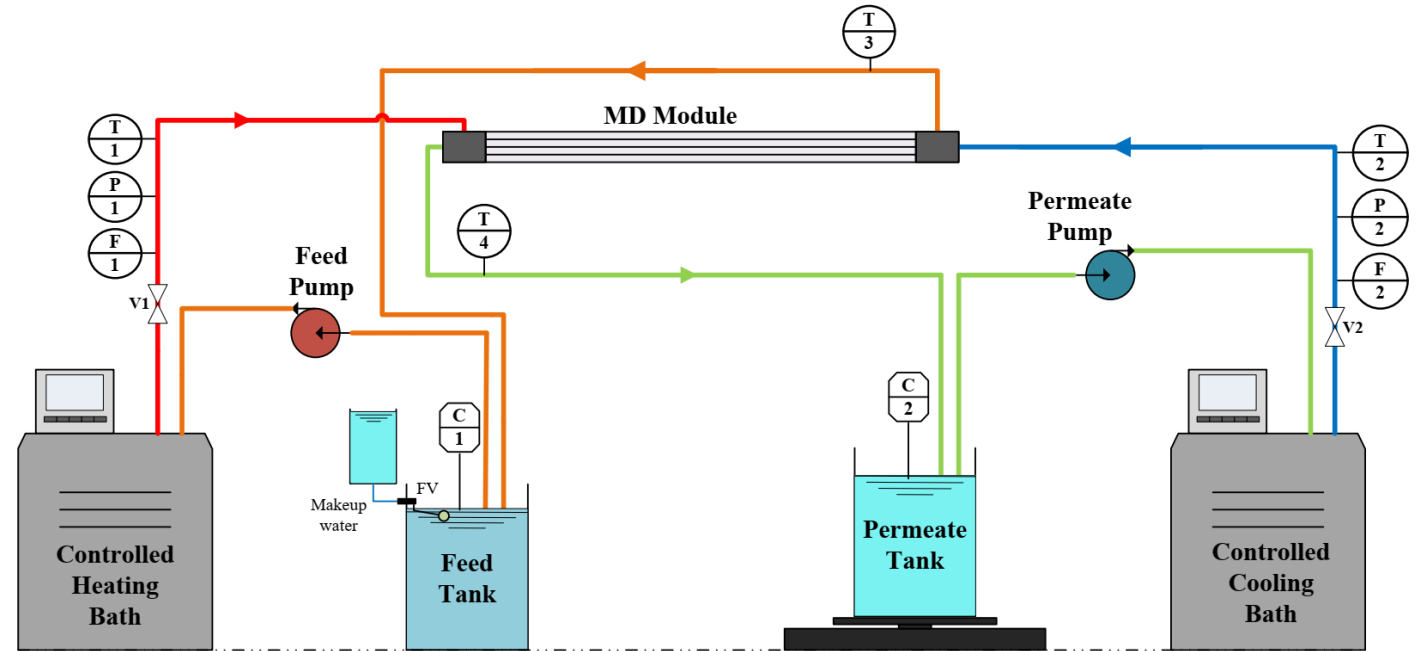
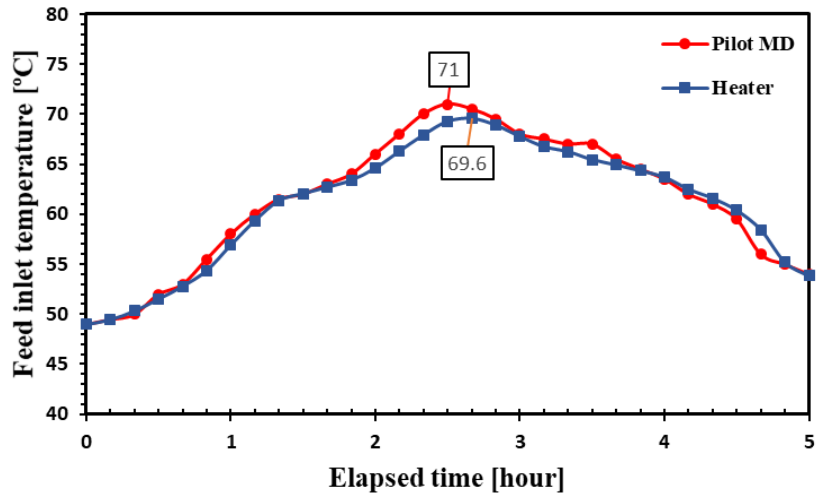
*(Drain protocol):*

The module is only drained from liquids at the shutdown event and left to dry overnight

**C**

*(On/Off protocol):*

The unit is turned off at the operation end while keeping the feed and permeate inside the module overnight



- T : Temperature sensor
- P : Pressure sensor
- F : Flow meter
- C : Conductivity meter
- V : Valve
- FV : Float valve





## Operating parameters

### Flow rates:

$$Q_f = 2.9 \text{ l/min}$$

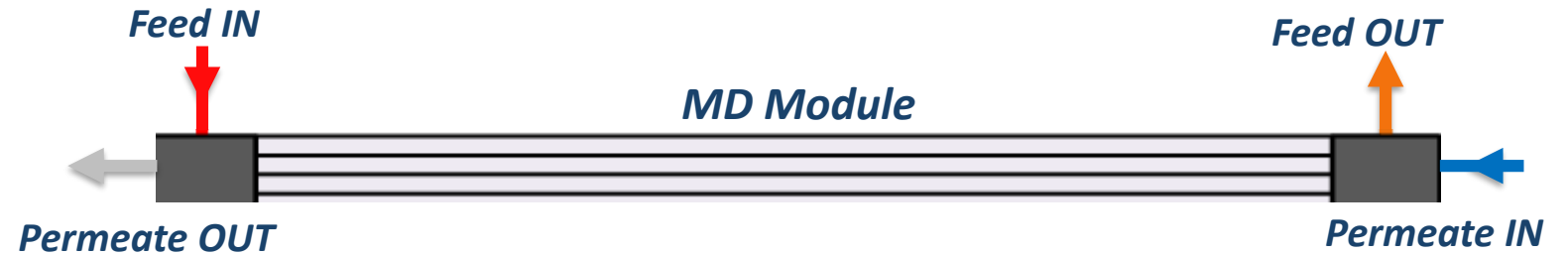
$$Q_p = 1 \text{ l/min}$$

### Permeate inlet temperature

$$T_p = 20 \text{ }^\circ\text{C}$$

### Feed inlet temperature

$$T_f = \text{variable}$$

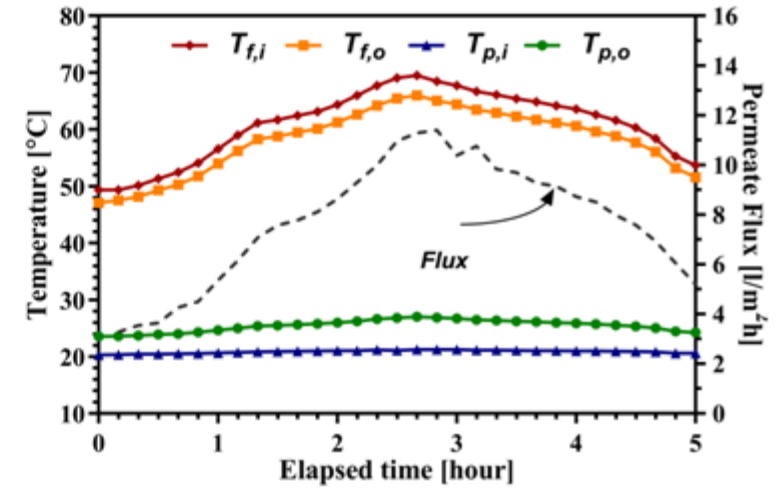
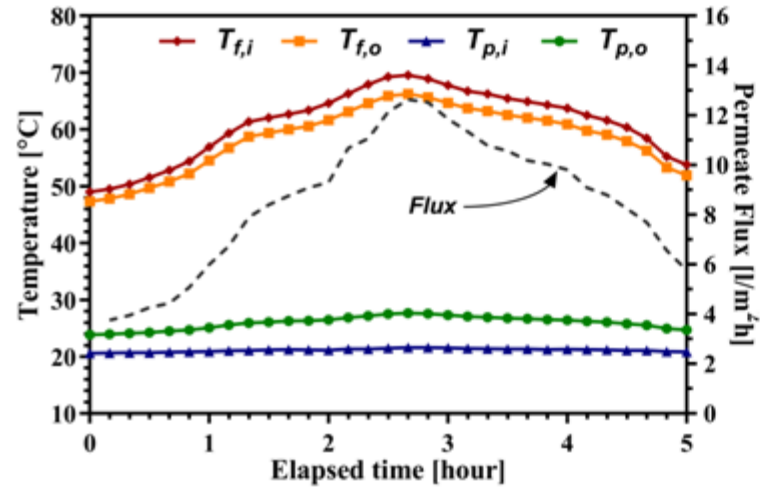


DCMD- hollow fiber module	Properties
Membrane material	PVDF
Number of hollow fibers	15
Nominal inner diameter of the fiber (mm)	0.75
Nominal outer diameter of the fiber (mm)	1.2
Mean pore size ( $\mu\text{m}$ )	0.1
Module diameter (mm)	12
Effective module length (m)	0.33
Effective module's membrane area ( $\text{m}^2$ )	0.018652



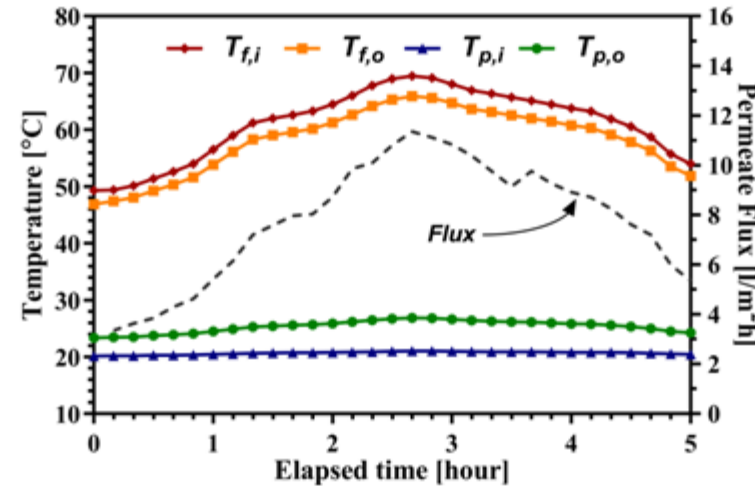
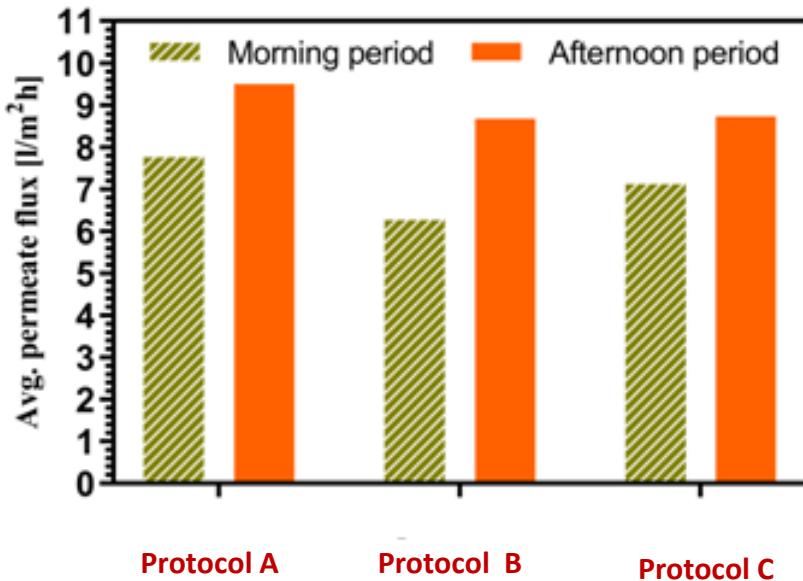


Inlet feed temperature and permeate flux profiles of the MD module for protocols A, B, and C during day 2



Protocol A

Protocol B



Protocol C



High permeate TDS values during the first hour of operation in experiments A and B (for day 7)

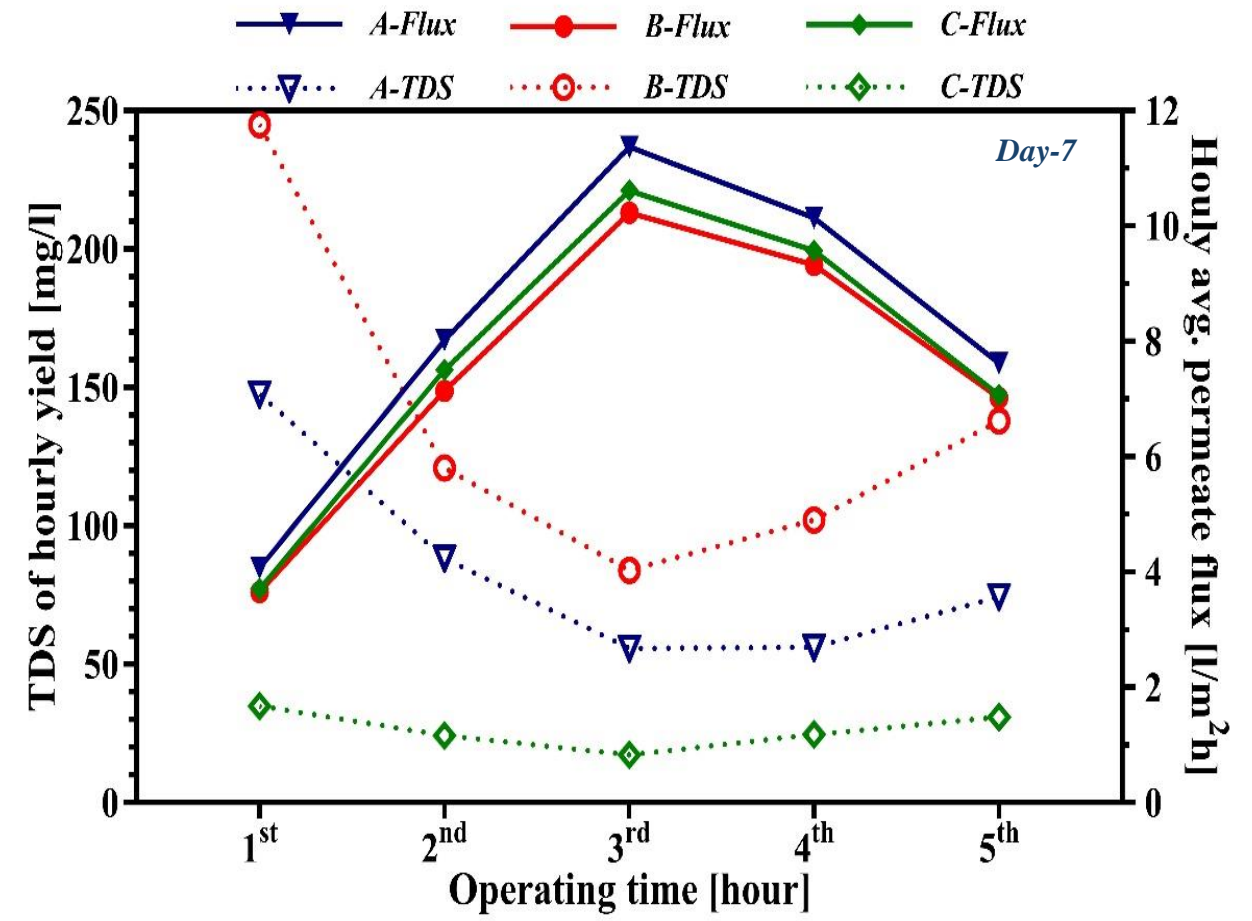
**1<sup>ST</sup> hour**  
**A 147 mg/l**  
**B 245 mg/l**

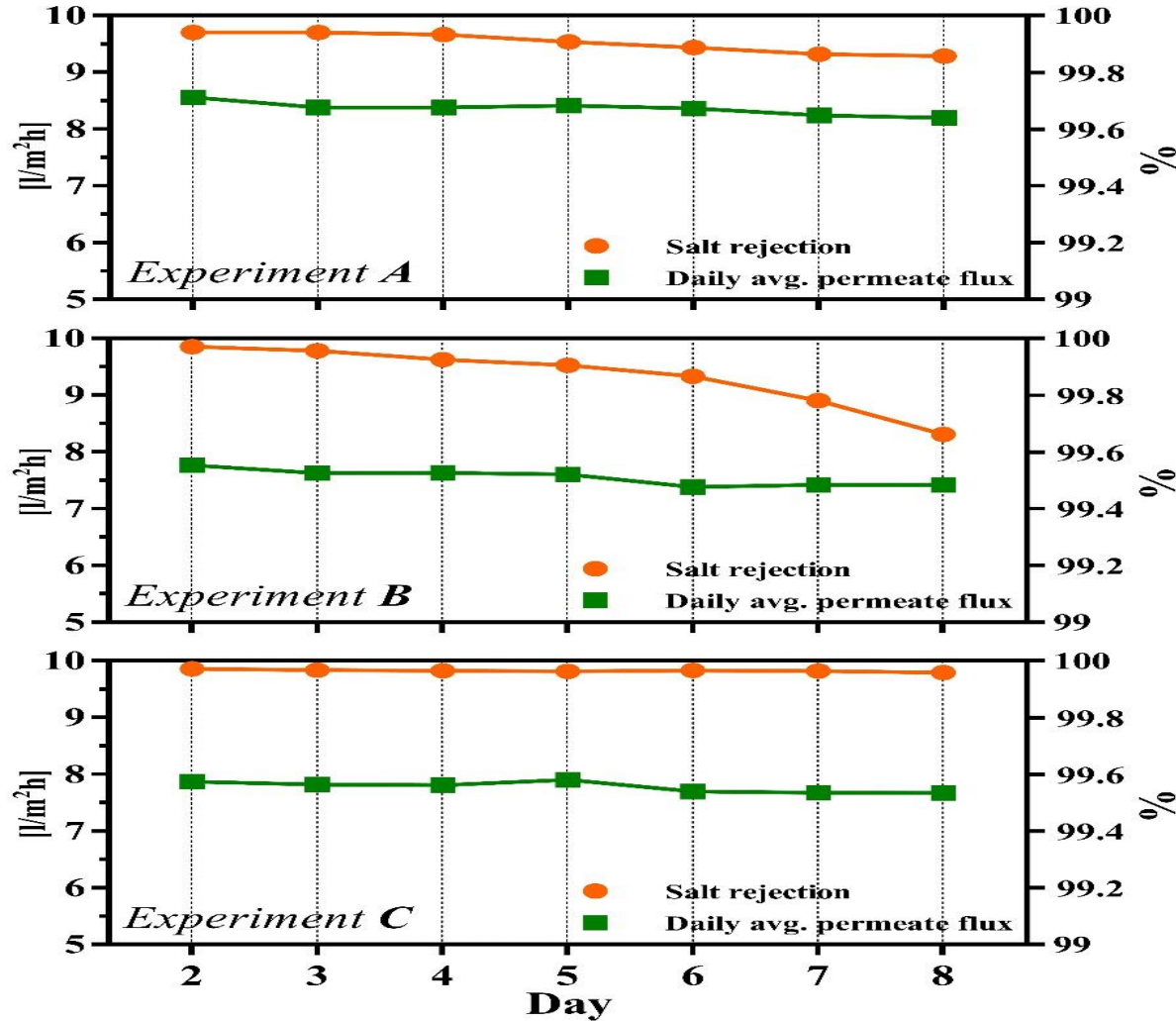


**3<sup>rd</sup> hour**  
**56 mg/l**  
**84 mg/l**

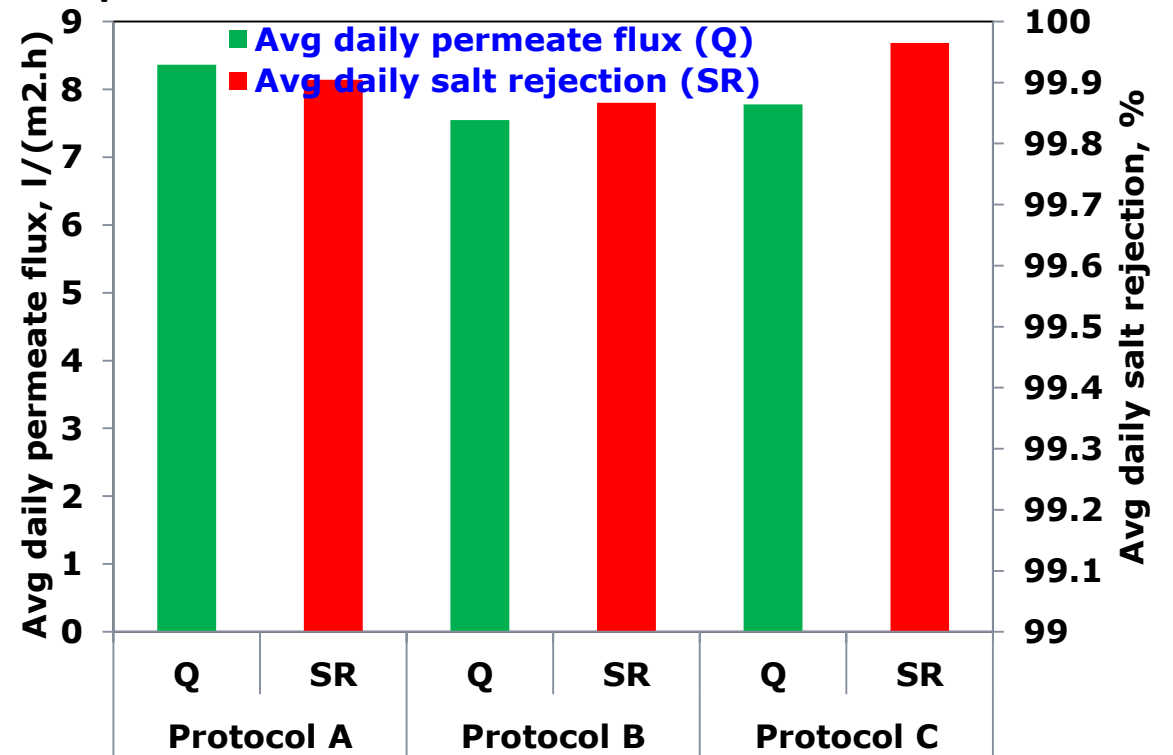
**Deposition of salt particles on the membrane surface due to dry out at night**

**A higher permeate vapor flux at elevated temperature results in greater dilution of any saline flux in liquid form through locally wetted pores**





- Insignificant variations in the average daily permeate flux between protocols
- Slight decrease in average daily permeate flux over time
- Gradual degradation in SR factor especially in protocol B

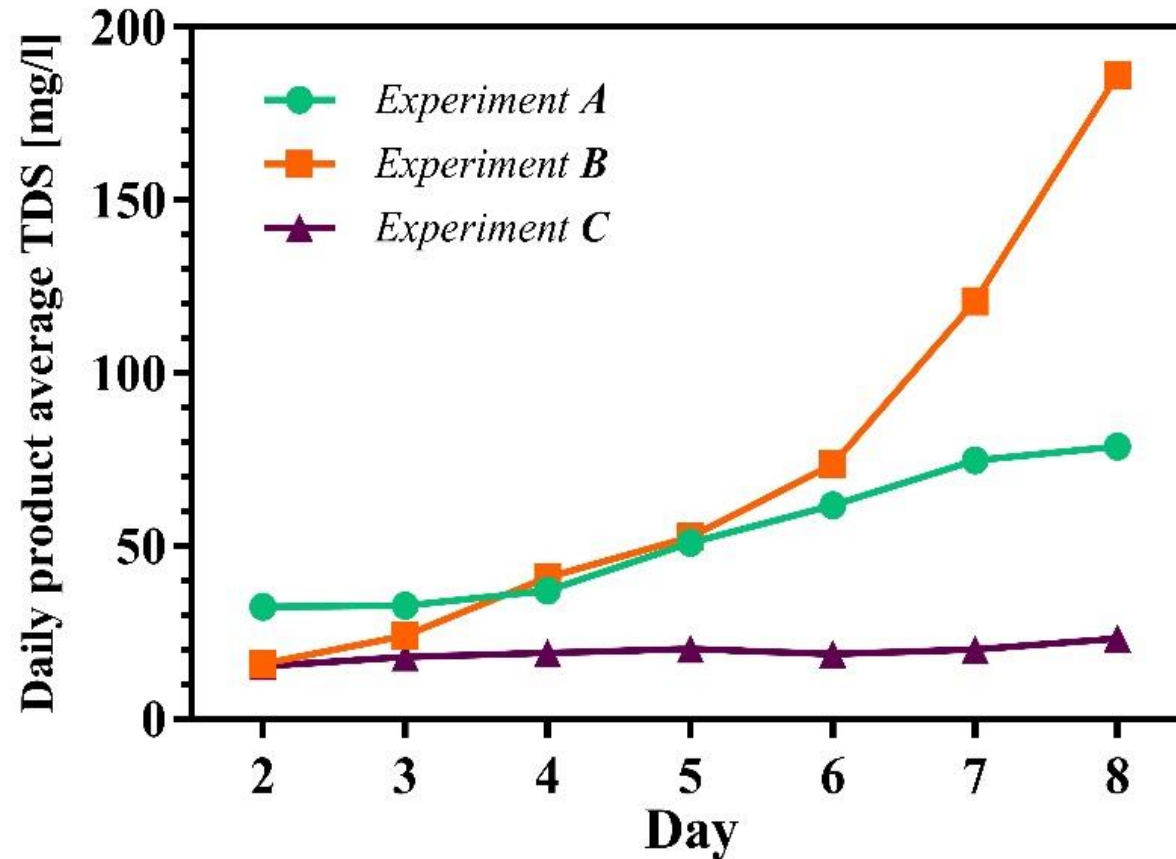






**Protocol B is less preferable:**

**Deposition of salt particles on the membrane surface due to dry out at night**







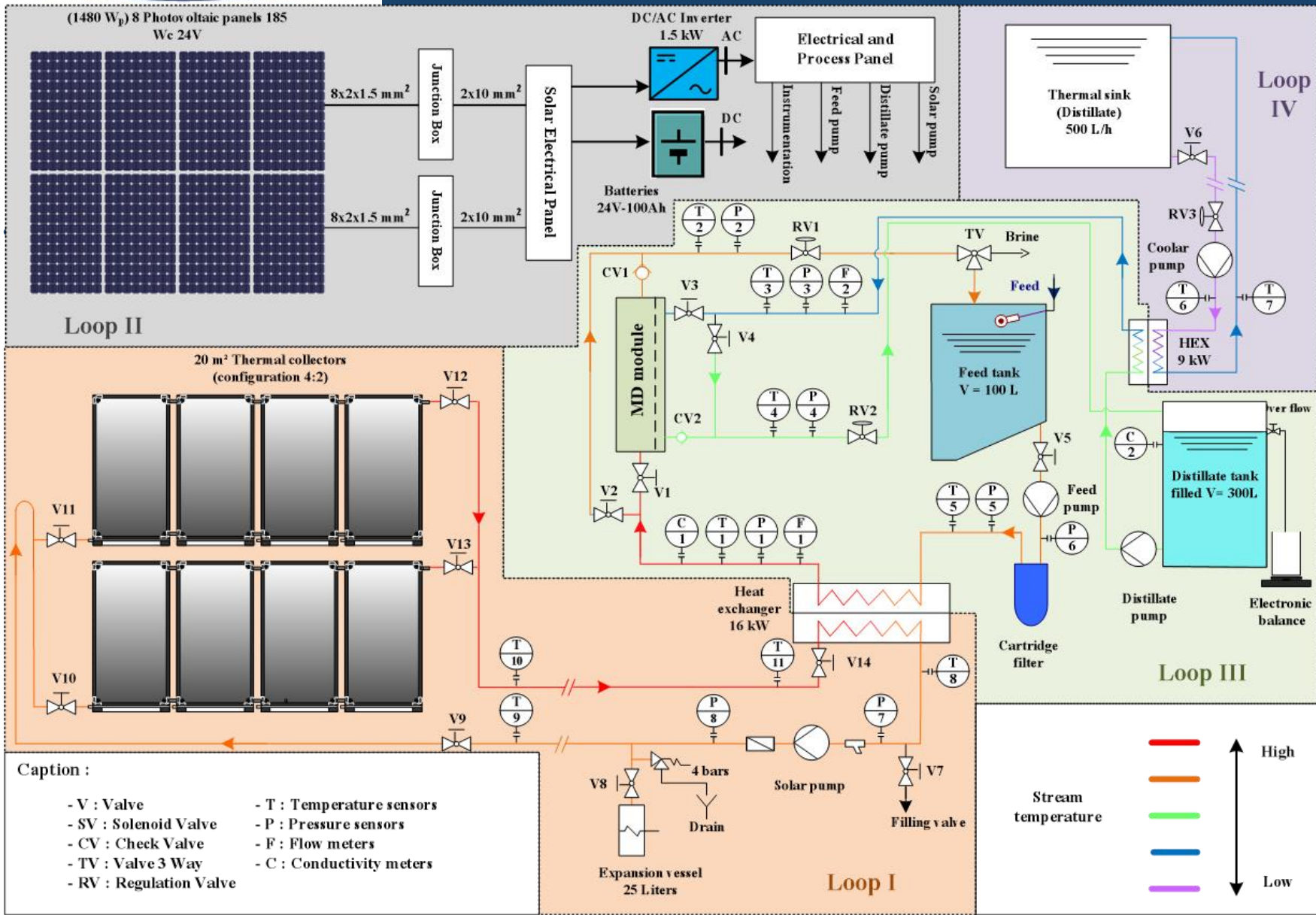
# Performance evaluation of a solar powered DCMD pilot unit under intermittent operation



**Thermal sink system**  
 2 water cooling units,  
 capacity of cold water tank  
 500 l, compressor H.P : 2.5,  
 cooling capacity : 1000  
 liters/h.  
 Heat exchanger: 9 kW



**PV system**  
 8 PV panels assembled in  
 parallel- peak capacity 1.480  
 kW<sub>peak</sub>  
 Electric batteries  
 DC/AC inverter  
**Solar collector system**  
 8 flat plate collectors arranged  
 in a series: parallel (4:2)  
 configuration- total effective  
 area 20 m<sup>2</sup>  
 Heat exchanger: 16 kW.



**Schematic diagram of the SPMD pilot unit**





## Specifications of the membrane module

<b>Module model</b>	<b>MICRODYN® - MD 063 CP 2N</b>
<b>Membrane material and type</b>	<b>Polypropylene/ Hollow fiber</b>
<b>Module configuration</b>	<b>Shell-and-tube</b>
<b>Number of fibers</b>	<b>200</b>
<b>Fibers inner diameter (mm)</b>	<b>1.8</b>
<b>Pore size (µm)</b>	<b>0.2</b>
<b>Membrane area (m<sup>2</sup>)</b>	<b>0.75</b>



**MICRODYN  
NADIR**

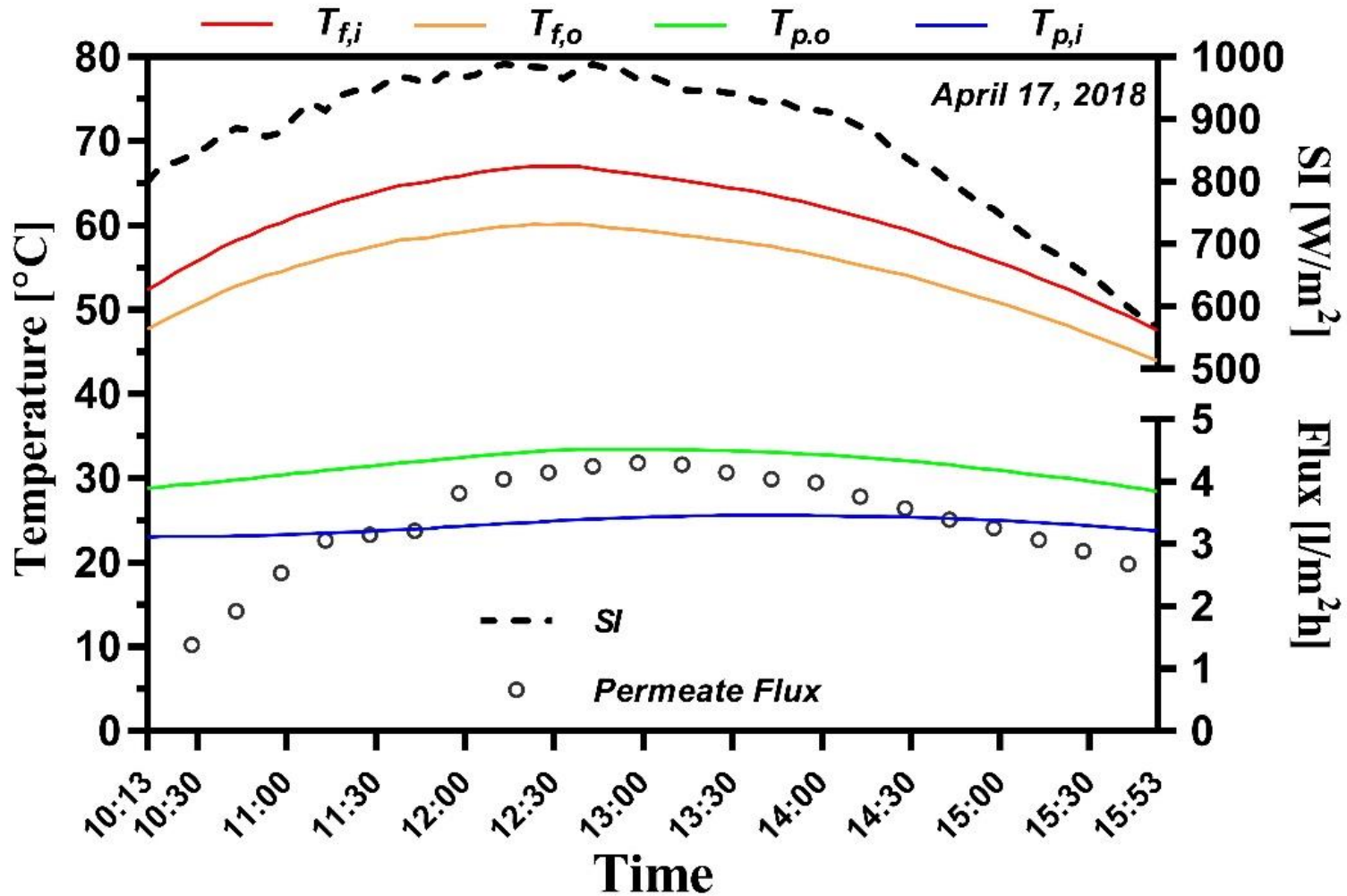
ADVANCED SEPARATION TECHNOLOGIES

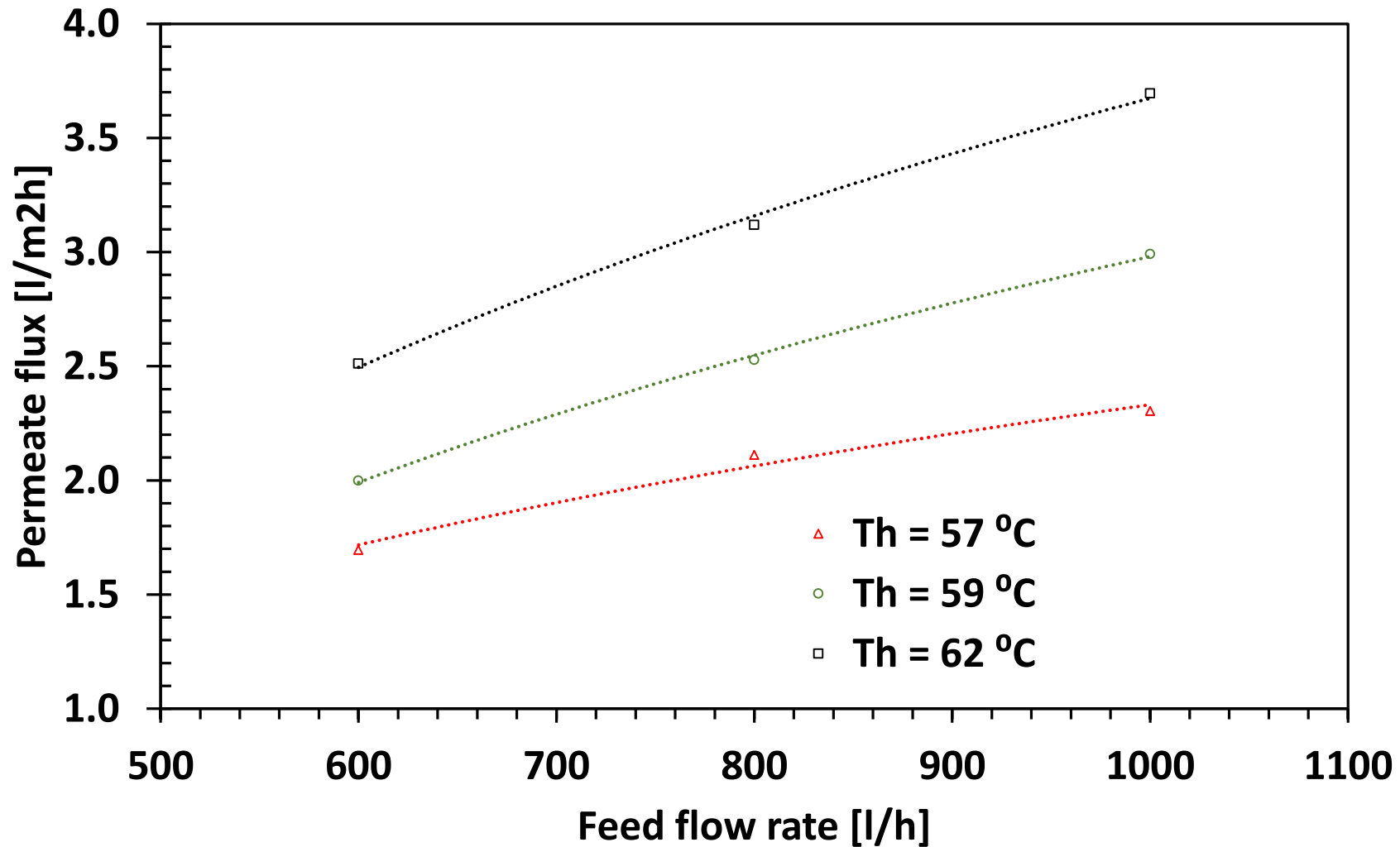


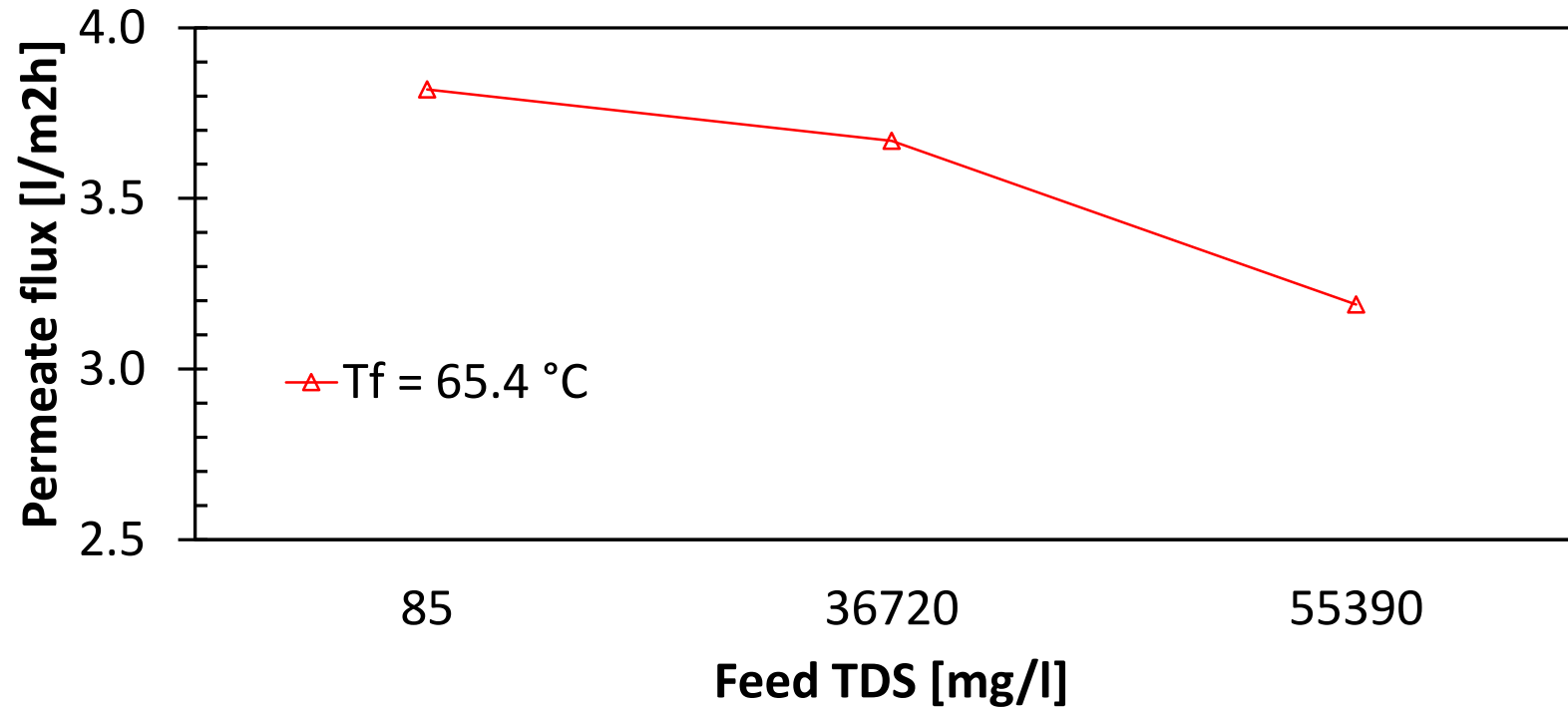
## Testing operating parameters

<b>Date of test</b>	<b>Type of feed water</b>	<b>Feed flow rate [l/h]</b>	<b>Permeate flow rate [l/h]</b>	<b>Feed temperature [°C]</b>	<b>Permeate temperature [°C]</b>
<b>April 16</b>	<b>Tap water</b>	<b>600</b>	<b>600</b>	<b>Variable with the solar radiation</b>	<b>23±1</b>
<b>April 17</b>	<b>Tap water</b>	<b>800</b>			
<b>April 18</b>	<b>Tap water</b>	<b>1000</b>			
<b>April 19</b>	<b>Seawater</b>	<b>800</b>			
<b>April 22</b>	<b>SWRO brine</b>	<b>800</b>			





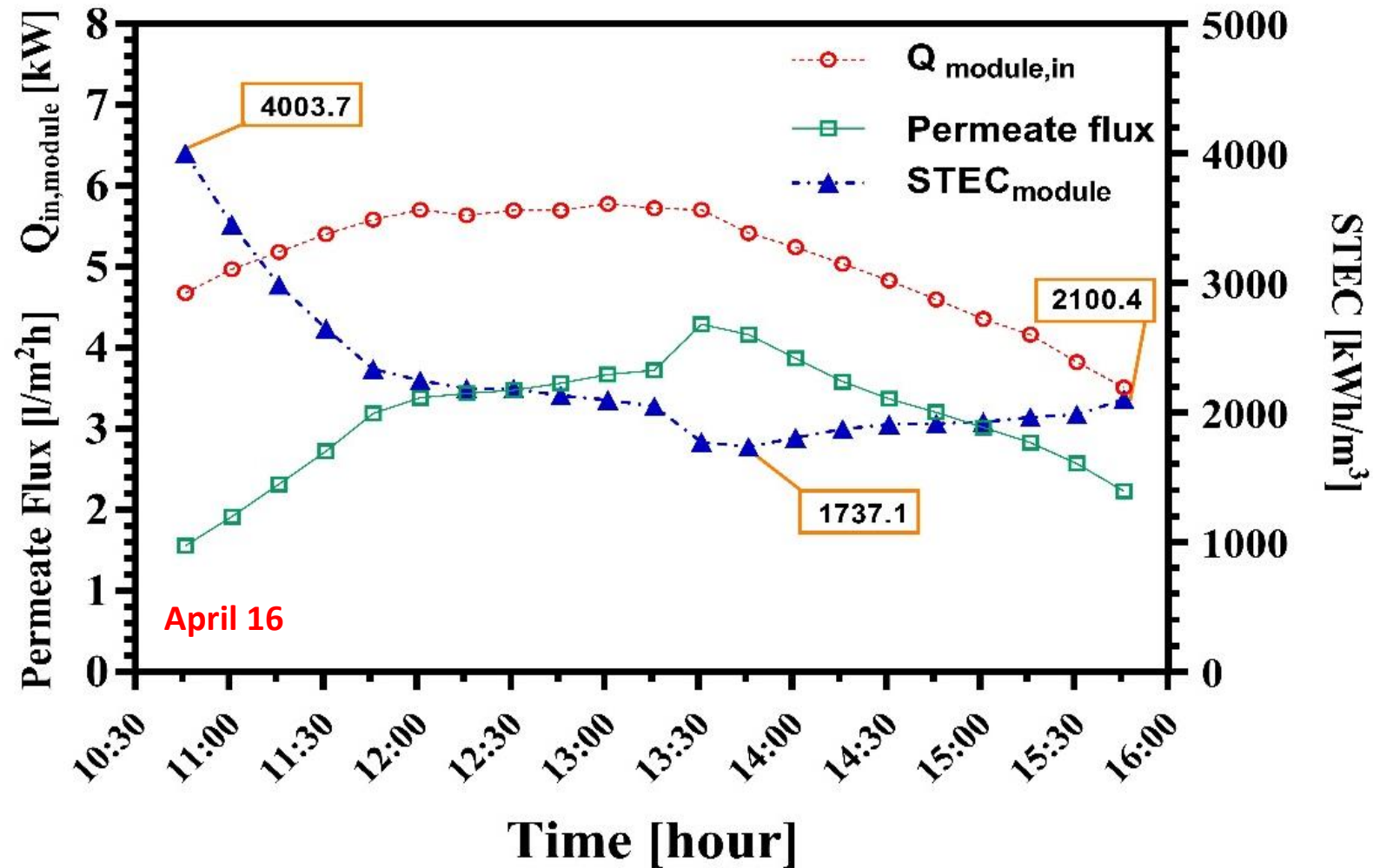




**16.5% decrease in the permeate flux when SWRO brine was used instead of tap water. Vapor pressure of water decreases with salt concentration increase.**



- STEC values high at the start.
- STEC values decreased during the first hour of operation and reached a minimum of 1737.1 kWh/m<sup>3</sup>

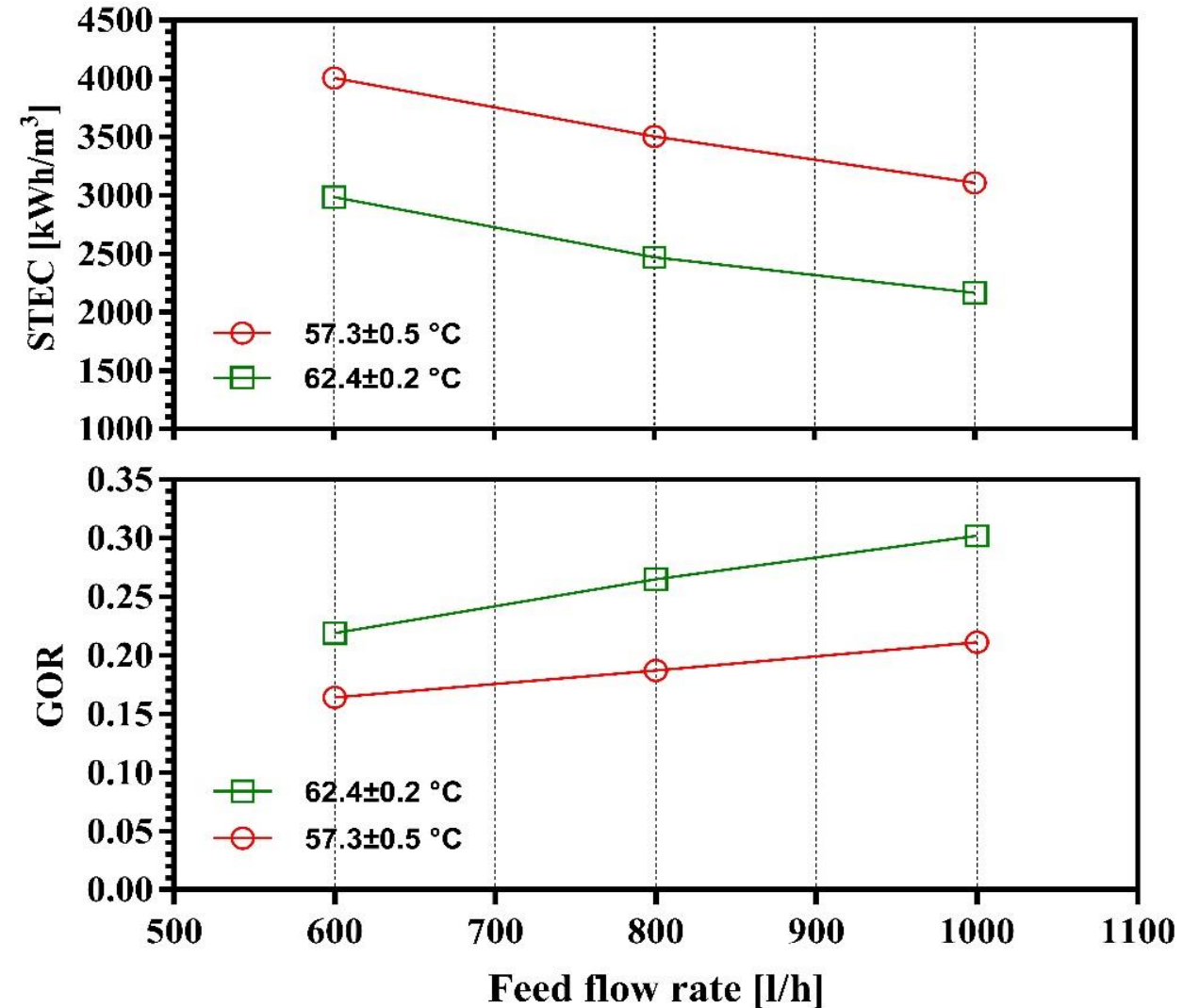




- Very low GOR values 0.12- 0.37 compared to other thermal desalination processes.
- Low performance and high energy consumption

## Limitations

- ❖ Low permeate flux rates
- ❖ High conductive heat loss of membrane module







- 1. The selection criteria for Intermittent operation protocol of SPMD should be based on their effects on the performance parameters and on their suitability for easy operation.**
- 2. The permeate flux was not affected by the type of intermittent operation protocol.**
- 3. The salt rejection is affected by the selected protocol and was low in case of drain without wash Protocol.**
- 4. The on/off Protocol was not only the easiest protocol but was also the best protocol with regard to performance parameters.**
- 5. The performance of hollow fiber DCMD module when operated on SPMD pilot system in terms of productivity and energy consumption was low.**



شكرا لكم

**Thank You**



**Center of Excellence  
in Desalination Technology**



**مركز التميز البحثي  
في تقنية تحلية المياه**



وزارة التعليم العالي  
MINISTRY OF HIGHER EDUCATION

الريادة في تقنية تحلية المياه  
Pioneering in Desalination Technology

الريادة في تقنية تحلية المياه  
Pioneering in Desalination Technology

معمل توصيف واختبار الأغشية  
Membrane characterization labs



معامل عمليات التحلية  
Desalination processes labs



معمل تصنيع الأغشية  
Membrane synthesis lab

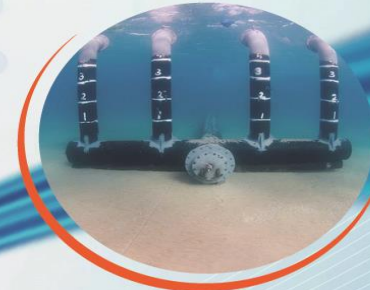


معمل تحليل المياه  
Water analysis lab

العمليات الحرارية لتحلية المياه  
Thermal desalination



خلية المياه بالطاقة الشمسية  
Solar-Driven Desalination



إدارة مياه الرجيع  
Brine management

خلية المياه بتقنية الأغشية  
Membrane desalination



معالجة مياه التغذية وانتساح الأغشية  
Feed water pretreatment and  
membrane fouling

